

Europäisches Patentamt European Patent Office Office européen des brevets



EP 0 757 069 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention of the grant of the patent: 25.09.2002 Bulletin 2002/39

(51) Int CI.7: **C08J 5/18**, C08L 23/12

(11)

(21) Application number: 96111738.9

(22) Date of filing: 20.07.1996

(54) Polypropylene blown film

Blasfolien aus Polypropylen
Feuilles gonflées de polypropylène

(84) Designated Contracting States:

AT BE DE DK ES FI FR GB IT NL PT SE

(30) Priority: 24.07.1995 US 505925

(43) Date of publication of application: 05.02.1997 Bulletin 1997/06

(73) Proprietor: Basell North America Inc. Elkton, Maryland 21921 (US)

(72) Inventors:

Giacobbe, James M.
 Wallingford, Pennsylvania 19086 (US)

Pufka, Steven J.
 Newark, Delaware 19702 (US)

(74) Representative:
Luderschmidt, Schüler & Partner GbR
Patentanwälte,
Postfach 3929
65029 Wiesbaden (DE)

(56) References cited:

EP-A- 0 477 662 EP-A- 0 651 010 EP-A- 0 573 862

US-A- 5 409 992

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

Description

[0001] This invention relates to blown thermoplastic films or sheets prepared from a broad molecular weight distribution propylene polymer material.

- [0002] Propylene homopolymers have been difficult to process on blown film extrusion equipment, since the inherent low melt strength of these polymers causes bubble instability and poor film gauge control. The range of processing conditions for polypropylene is quite narrow and difficult to control. The addition of an ethylene copolymer, such as an ethylene/propylene copolymer, aids in control of the film bubble, since ethylene homopolymers and copolymers process well on this type of equipment. However, the processing of such copolymers is still quite sensitive.
- [0003] U.S.P. 5,318,842 discloses a film or sheet comprising (a) a film or sheet of a crystalline homopolymer of a 3-10 carbon alpha-olefin monomer or certain propylene copolymers, and (b) at least one surface layer of a broad molecular weight distribution propylene polymer material. The multilayer films are coextruded and biaxially oriented. U.S.P. 5,409,992 discloses blends of (a) a heterophasic olefin polymer material, and (b) a broad molecular weight distribution propylene polymer material, and their use for making calendered films and sheets.
- [0004] EP 0 573 862 describes crystalline polymers and copolymers of propylene having a molecular weight distribution $M_w/M_n > 20$, a melt flow rate MFR > 2 dg/min and a content of fraction insoluble in xylene at 25°C \geq 94. Said polymers are said to be particularly adequate for the extrusion of thin sheets to be subjected to thermoforming, as well as for injection molding and blow molding processes. However neither of these references discloses the manufacture of blown film from broad molecular weight distribution propylene polymer materials.
- 20 [0005] A propylene polymer that could be used to produce blown film with a stable film bubble and the capability for tight film gauge control would be desirable.
 - [0006] The film or sheet material of this invention comprises a broad molecular weight distribution propylene polymer material having a molecular weight distribution M_w/M_n of 4 to 20, a melt flow rate of 0.5 to 2 dg/min, and xylene insolubles at 25°C of greater than or equal to 94%, wherein the film or sheet is a blown film or sheet. The broad molecular weight distribution propylene polymer material can be, for example, a broad molecular weight distribution propylene rubber impact-modified propylene homopolymer, wherein the propylene homopolymer has a broad molecular weight distribution.
 - [0007] The broad molecular weight distribution propylene polymer material has increased melt strength and modulus compared to previously available propylene homopolymer. It has been found that this polymer can be used to produce blown film, since a stable film bubble is formed and film gauge can be controlled. Blown films made from a blend of this broad molecular weight distribution propylene polymer material and a heterophasic olefin polymer composition have increased impact and tear resistance.
 - [0008] The propylene polymer material used for making the blown film of this invention has a broad molecular weight distribution M_w/M_n of 4 to 20; a melt flow rate of 0.5 to 2 dg/min, and xylene insolubles at 25°C of greater than or equal to 94%, preferably greater than or equal to 96%. This broad molecular weight distribution polymer has increased melt strength and modulus compared to currently available propylene homopolymer. For example, currently available propylene homopolymer has a flexural modulus of 1,680 to 1,750 MPa [240,000 to 250,000 psi], while the propylene homopolymer used for making the blown films of this invention typically has a flexural modulus of 2,100 MPa [300,000 psi].
 - [0009] The broad molecular weight distribution propylene polymer material can be, for example, a broad molecular weight propylene homopolymer, or an ethylene/propylene rubber impact-modified broad molecular weight distribution propylene homopolymer. When the propylene polymer material is an ethylene/propylene rubber impact-modified broad molecular weight distribution propylene homopolymer, the propylene homopolymer has the same properties as those listed in the previous paragraph, i.e., a molecular weight distribution M_w/M_n of 4 to 20; a melt flow rate of 0.5 to 2 dg/min, and xylene insolubles at 25° C of greater than or equal to 94%, preferably greater than or equal to 96%.
 - [0010] The broad molecular weight distribution propylene polymer material described above can be prepared by sequential polymerization in at least two stages, in the presence of a Ziegler-Natta catalyst supported on magnesium halides in active form. Preferably the catalyst contains as an essential element a solid catalyst component (a) comprising a titanium compound having at least one titanium-halogen bond, and an electron donor compound, both supported on a magnesium halide in active form. The catalyst is capable of producing propylene polymers having a xylene insolubles fraction at 25°C greater than or equal to 94%, preferably greater than or equal to 96%, and has a sensitivity to molecular weight regulators high enough to produce propylene homopolymer having a melt flow rate (MFR) of less than or equal to 0.5 and greater than or equal to 50 dg/min.
 - [0011] The catalysts used are obtained by contacting
 - (a) the solid catalyst component mentioned above,
 - (b) an aluminum alkyl compound, and
 - (c) an external electron donor compound.

55

- [0012] Solid catalyst components (a) having the characteristics mentioned above are well known in the patent literature. Particularly suited are the solid catalyst components described in U.S.P. 4,339,054 and European Patent 45,977. Other examples can be found in U.S.P. 4,472,524.
- [0013] In general, the solid catalyst components used in the catalysts comprise, as electron donor compounds, compounds selected from ethers, ketones, and lactones; compounds containing N, P, and/or S atoms, and esters of monoand dicarboxylic acids.
- [0014] Particularly suited are the esters of phthalic acid, such as diisobutyl, dioctyl and diphenyl phthalate, and benzyl butyl phthalate; the esters of malonic acid, such as diisobutyl and diethyl malonate; the alkyl and aryl pivalates; the alkyl, cycloalkyl and aryl maleates; alkyl and aryl carbonates such as diisobutyl carbonate, ethyl phenyl carbonate, and diphenyl carbonate, and the esters of succinic acid, such as mono- and diethyl succinate.
- [0015] The preparation of these catalysts can be carried out according to several methods. For example, the magnesium halide (anhydrous, i.e., containing less than 1% of water), the titanium compounds, and the electron donor compound can be milled under conditions where the magnesium halide is active. The milled product is then treated one or more times with an excess of TiCl₄ at temperatures from 80° to 135°C, after which it is washed repeatedly with a hydrocarbon, such as hexane, until all of the chlorine ions have been removed.
- [0016] According to another method, the anhydrous magesium halide is preactivated according to known methods, and then caused to react with an excess of TiCl₄ containing the electron donor compound in solution. The treatment takes place at temperatures ranging from 80° to 135°C. Optionally, the treatment with TiCl₄ is repeated, and the solid washed with hexane, or another hydrocarbon solvent, in order to eliminate all traces of unreacted TiCl₄.
- [0017] According to another method, a MgCl₂.nROH adduct (in particular in the form of spheroidal particles), where n is generally from 1 to 3, and ROH is ethanol, butanol, or isobutanol, is reacted with an excess of TiCl₄ containing the electron donor compound in solution. The temperature generally ranges from 80°C to 120°C. The solid is then isolated and reacted once more with the TiCl₄, after which it is separated and washed with a hydrocarbon until all chlorine ions have been removed.
- [0018] According to another method, magnesium alcoholates and chloroalcoholates (particularly the chloroalcoholates prepared according to the method described in U.S.P. 4,220,554) are reacted with an excess of TiCl₄ containing the electron donor compound in solution, carried out according to the reaction conditions described above.
 - [0019] In the solid catalyst component (a), the titanium compound expressed as Ti is generally present in a percentage ranging from 0.5 to 10% by weight. The quantity of electron donor compound that remains fixed on the solid component (internal donor), generally ranges from 5 to 20 mole % with respect to the magnesium dihalide.
 - **[0020]** The titanium compounds that can be used for the preparation of the solid catalyst component (a) are the halides and the halogen alcoholates. Titanium tetrachloride is the preferred compound. Satisfactory results can also be obtained with titanium trihalides, particularly TiCl₃OR, where R is a phenyl radical.
 - [0021] The reactions indicated above bring about the formation of magnesium halide in active form. Besides these reactions, other reactions are known in the literature that cause the formation of activated magnesium halide starting from magnesium compounds other than the halides, such as carboxylates of magnesium, for example.
 - [0022] The active form of the magnesium halides in the catalyst component (a) can be identified by the X-ray spectrum of the catalyst component wherein the major intensity reflection, which appears on the spectrum of the nonactivated magnesium chloride (having a surface area smaller than 3 m²/g), is no longer present, but in its place there is a halo with the maximum intensity shifted with respect to the position of the major intensity reflection of the nonactivated magnesium dihalide, or by the fact that the major intensity reflection shows a width at half-height at least 30% greater than the one of the major intensity reflection that appears in the nonactivated magnesium chloride spectrum.
 - [0023] The most active forms are those where the halo mentioned above appears in the X-ray spectrum of the component.
- 45 [0024] Among the magnesium halides, the chloride is the preferred compound. In the case of the most active forms of magnesium chloride, the X-ray spectrum of the catalyst component shows a halo instead of the reflection that in the spectrum of the nonactivated chloride appears at a distance of 2.56Å.
 - [0025] The aluminum alkyl compounds (b) used as co-catalysts comprise the aluminum trialkyls, such as Al triethyl, Al isobutyl, Al-tri-n-butyl, and linear or cyclic aluminum alkyl compounds containing two or more aluminum atoms bonded through O or N atoms, or SO₄ and SO₃ groups.
 - [0026] Examples of these compounds are:

55

CH₃
|
(C₂H₃)₂Al=SO₂-Al(C₂H₃)₂; CH₃(Al=O-)-Al(CH₃)₃;

where n is a number from 1 to 20.

10

15

20

25

[0027] The aluminum alkyl compound is generally used in such quantities that the Al/Ti ratio ranges from 1 to 1000. [0028] In addition to the solid catalyst component (a) and the aluminum alkyl compound (b), the catalysts contain an external electron donor compound (c). The external electron donor compound is selected from silanes capable of conferring to the polymer product produced by the catalyst the levels of stereospecificity mentioned above (determined by the high content of xylene insolubles at 25°C) and sensitivity to whatever molecular weight regulator is used.

[0029] Suitable for this purpose are the silanes containing at least one cyclopentyl group bonded to the silicon, and one or more -OR groups also bonded to the silicon atom, where R is a 1-18 carbon alkyl, 3-18 carbon cycloalkyl, 6-18 carbon aryl, or 7-18 carbon aralkyl radical. Preferably R is methyl or ethyl. Particularly suited is dicyclopentyldimethoxysilane. The external donors mentioned above are generally used in quantities ranging from 0.001 to 15 moles, preferably from 1 to 10 moles with respect to the moles of aluminum alkyl compound (b).

[0030] The sequential polymerization is carried out in the presence of the above catalysts, and the polymerization occurs in at least two stages. Fraction (A) and (B) are prepared in separate and consecutive stages, in each stage in the presence of the polymer and the catalyst from the preceding stage.

[0031] The polymerization process can be carried out in a batch or continuous mode according to known techniques, operating in liquid phase in the presence or absence of an inert diluent, or in gas phase, or liquid-gas phase. Gas phase is preferred.

[0032] The polymerization reaction times and temperatures are not critical, however, it is preferred that the polymerization is carried out at a temperature of from 20°C to 100°C.

[0033] The regulation of the molecular weight is controlled using known regulators, particularly hydrogen.

[0034] The catalysts can be precontacted with small quantities of olefins (prepolymerization). Prepolymerization improves both catalyst activity and polymer morphology.

[0035] Prepolymerization is carried out by maintaining the catalyst in suspension in a hydrocarbon (hexane or heptane, for example) for a period of time that is sufficient to produce a quantity of polymer ranging from 0.5 to 3 times the weight of the solid component. The polymerization temperature is between ambient temperature and 60°C. Prepolymerization can also be carried out in liquid propylene under the temperature conditions described above. Quantities of polymer that can reach 1000 g per g of catalyst component are produced.

[0036] The broad molecular weight distribution propylene homopolymer can also be blended with 10% to 90% by weight, based on the total weight of the composition, of a heterophasic olefin polymer composition to give a film with increased impact and tear resistance. The amount of heterophasic olefin polymer composition used depends upon the film properties that are desired. The heterophasic olefin polymer composition is prepared by polymerization in at least two stages and comprises

5

10

15

40

45

50

(a) from 10 to 50 parts of a propylene homopolymer having an isotactic index greater than 80, or a copolymer selected from the group consisting of(i) propylene and ethylene, (ii) propylene, ethylene and a CH₂=CHR alphaolefin, where R is a C₂₋₈ straight or branched alkyl, and (iii) propylene and an alpha-olefin as defined in (ii), said copolymer containing over 80% propylene and having an isotactic index greater than 80;

(b) from 5 to 20 parts of a semi-crystalline, essentially linear copolymer fraction having a crystallinity of 20% to 60%, wherein the copolymer is selected from the group consisting of (i) ethylene and propylene containing over 55% ethylene, (ii) ethylene, propylene, and an alpha-olefin as defined in (a) (ii) containing from 1 to 10% of the alpha-olefin and over 55% of both ethylene and alpha-olefin, and (iii) ethylene and an alpha-olefin as defined in (a) (ii) containing over 55% of said alpha-olefin, which copolymer is insoluble in xylene at room or ambient temperature; and

(c) from 40 to 80 parts of a copolymer fraction wherein the copolymer is selected from the group consisting of (i) ethylene and propylene containing from 20% to less than 40% ethylene, (ii) ethylene, propylene, and an alphaolefin as defined in (a) (ii), wherein the alphaolefin is present in an amount of 1 to 10% and the amount of ethylene and alphaolefin present is from 20% to less than 40%, and (iii) ethylene and an alphaolefin as defined in (a) (ii) containing from 20% to less than 40% of said alphaolefin, and optionally with 0.5 to 10% of a diene, said copolymer fraction being soluble in xylene at ambient temperature, and having an intrinsic viscosity of from 1.5 to 4.0 dl/g;

with the total of the (b) and (c) fractions, based on the total olefin polymer composition, being from 50% to 90%, and the weight ratio of (b)/(c) being less than 0.4, wherein said composition has a flexural modulus of less than 150 MPa. [0037] The preparation of the heterophasic olefin polymer composition is disclosed in U.S.P. 5,212,246, the process of which is incorporated herein by reference.

[0038] The film or sheet material of this invention can also contain various additives known to those skilled in the art, such as, for example, fillers such as talc and calcium carbonate, pigments, antioxidants, slip agents, and antiblock agents.

[0039] The melt flow rate of the propylene polymer material was measured using ASTM D-1238, condition L.

[0040] Xylene insolubles were determined by dissolving 2 g of polymer in 200 ml of xylene at 135°C, cooling in a constant temperature bath to 22°C, and filtering through fast filter paper. An aliquot of the filtrate was evaporated to dryness, the residue weighed, and the weight % soluble fraction calculated.

[0041] Molecular weight distribution M_w/M_n was determined using a Waters 150-C ALC/gel permeation chromatograph in trichlorobenzene at 145°C with a differential refractive index detector.

[0042] The film-forming material was stabilized with 0.1 pph calcium stearate, 0.2 pph Irganox B225 stabilizer available from Ciba Geigy (a 1:1 blend of Irgafos 168 phosphite stabilizer and Irganox 1010 hindered phenolic stabilizer), 0.3 pph Sylobloc 45 antiblocking agent, available from W. R Grace, and 0.3 pph Kemamide E slip additive, available from Croda. The air quenched blown film was prepared by charging the composition into a single screw extruder, extruding it through a circular die and blowing it into a film with a sufficient amount of air to provide a film of either 0.0254 or 0.0508 mm [1 or 2 mils] thickness using the following equipment and processing conditions. In the table, fpm = feet per minute.

| Barrel Temperature Profile | | | | |
|----------------------------|---------------------|--|--|--|
| Zone 1 | 210°C [410°F] | | | |
| Zone 2 | 210°C [410°F] | | | |
| Zone 3 | 210°C [410°F] | | | |
| Zone 4 | 210°C [410°F] | | | |
| Die temperature | 218°C [425°F] | | | |
| Melt temperature | 221°C [430°F] | | | |
| Die pressure | 10.5 MPa [1500 psi] | | | |
| Die gap | 0,965 mm [0.038 in] | | | |
| Line speed | 15.5 m/min [51 fpm] | | | |

[0043] Although air quenched films were produced and tested in the following examples, it should be noted that the films could also have been subjected to water quenching instead of air quenching.

[0044] The tests used to measure the properties of the resulting film were: tensile strength at yield (ASTM D-638), tensile strength at break (ASTM D-638), tensile elongation at yield (ASTM D-638), tensile elongation at break (ASTM D-638), dart drop impact (ASTM D-4272-83), and 2% secant modulus (ASTM D-882).

[0045] In this specification all parts and percentages are by weight unless otherwise noted.

Example 1

10

15

20

25

30

40

45

50

55

[0046] A film having a thicknes of 0.0254 mm [1 mil] was prepared as described above from a broad molecular weight distribution propylene homopolymer having a MFR of 3.8 dg/min, 98.4% insolubles in xylene at room temperature, and $M_w/M_n = 13.9$. The physical properties of the film are given in Table 1.

Table 1

| Tensile Strength @ Yield | |
|----------------------------|-----------------|
| MD (MPa) [psi] | 44.3 [6,330] |
| CD (MPa) [psi] | 34.3 [4,900] |
| Tensile Elongation @ Yield | |
| MD(%) | 4.4 |
| CD (%) | 3.1 |
| Tensile Strength @ Break | |
| MD (MPa) [psi] | 76.8 [10,965] |
| CD (MPa) [psi] | 34.3 [4,900] |
| Tensile Elongation @ Break | |
| MD (%) | 460 |
| CD (%) | 3 |
| 2 % Secant Modulus | |
| MD (MPa) [psi] | 1,390 [198,570] |
| CD (MPa) [psi] | 1,235 [176,400] |
| | |

Example 2

[0047] Films having thicknesses of 1 mil and 2 mils were prepared from blends of broad molecular weight distribution propylene homopolymer and a heterophasic olefin polymer composition, using varying amounts of the two components of the blend. The amounts of each component in the blend and the physical properties of films made from the blends are given in Table 2. The additives and extrusion processing conditions were the same as in Example 1.

[0048] In the table, A is a heterophasic olefin polymer composition having a melt flow rate of 0.8 dg/min. The propylene homopolymer content of the heterophasic composition is 35%, the content of semi-crystalline, linear ethylene copolymer fraction is 5%, and the content of the ethylene copolymer fraction soluble in xylene is 60% by weight; based onthe total weight of the composition. B is a broad molecular weight distribution propylene homopolymer having a MFR of 1.2 dg/min, a molecular weight distribution M_w/M_n of 4.2, and xylene insolubles at 25°C of 98.7%.

Table 2

| | | IdDIC 2 | | | | |
|---|------------------------------------|------------------------------------|------------------------------------|-----------------------------------|------------------------------------|-----------------------------------|
| Ratio of polymers in blend (A/B) (%) | 30/70 | 30/70 | 50/50 | 50/50 | 70/30 | 70/30 |
| Film Thickness (mm) [mils] | 0.0254 [1.00] | 0.0508 [1.00] | 0.0254 [1.00] | 0.0508 [1.00] | 0.0254 [1.00] | 0.0508 [1.00] |
| Dart Drop Impact (grams) | <45 | 59 | 51 | 201 | 108 | 300 |
| Elmendorf Tear Strength @ Yield MD/ CD (grams) | 2/420 | 12/630 | 5/450 | 19/570 | 5/620 | 27/760 |
| Tensile Strength @ Yield MD/CD (MPa) [psi] | 42.0 [6000] /30.6 [4370] | 33.8 [4830] /26.3 [3760]. | 37.7 [5390] /22.4 [3200] | 29.5 [4210] /22.5 [3210] | 30.0 [4280] /16.9 [2420] | 21.5 [3070] /15.8 [2260] |
| Tensile Strength @ Break MD/CD (MPa) [psi] | 72.1 [10300] /30.7 [4390] | 59.5 [8500] /27.5 [3930] | 86.6 [12370]/ 22.5 [3210] | 57,4 [8200] /26.2 [3740] | 70.7 [10100] /21.3 [3040] | 45.5 [6500] /20.7 [2960] |

Table 2 (continued)

| Elongation @ Yield MD/CD (%) | 34/6 | 30/8 | 44/12 | 39/17 | 48/16 | 46/26 |
|---|--|---------------------------------------|-------------------------------------|-------------------------------------|-------------------------------------|-------------------------------------|
| Elongation @ Break MD/CD (%) | 441/41 | 540/520 | 530/540 | 540/540 | 480/540 | 540/540 |
| 2 % Secant Modulus MD/CD (MPa) [psi] | 1008 [144,000] /966 [138,000] | 819 [117,000] /812 [116,000] | 616 [88,000] /658 [94,000] | 581 [83,000] /595 [85,000] | 413 [59,000] /455 [65,000] | 357 [51,000] /371 [53,000] |

Claims

5

10

15

25

30

35

40

45

- 1. A film or sheet material comprising a broad molecular weight distribution propylene polymer material having a molecular weight distribution M_W/M_N of 4 to 20, a melt flow rate of 0.5 to 2 dg/min, and xylene insolubles at 25 °C of greater than or equal to 94 %, wherein the film or sheet is a blown film or sheet.
- 2. The film or sheet material of claim 1, wherein the broad molecular weight distribution propylene polymer material is a broad molecular weight distribution propylene homopolymer, or an ethylene/propylene rubber impact-modified broad molecular weight distribution propylene homopolymer.
 - 3. The film or sheet of claim 1, wherein the film or sheet material additionally comprises from 10% to 90%, based on the total weight of the composition, of a heterophasic olefin polymer composition prepared by polymerization in at least two stages and comprising
 - (a) from 10 to 50 parts of a propylene homopolymer having an isotactic index greater than 80, or a copolymer selected from the group consisting of(i) propylene and ethylene, (ii) propylene, ethylene and a CH_2 =CHR alpha-olefin, where R is a C_{2-8} straight or branched alkyl, and (iii) propylene and an alpha-olefin as defined in (ii), said copolymer containing over 80% propylene and having an isotactic index greater than 80;
 - (b) from 5 to 20 parts of a semi-crystalline, essentially linear copolymer fraction having a crystallinity of 20% to 60%, wherein the copolymer is selected from the group consisting of(i) ethylene and propylene containing over 55% ethylene, (ii) ethylene, propylene, and an alpha-olefin as defined in (a) (ii) containing from 1 to 10% of the alpha-olefin and over 55% of both ethylene and alpha-olefin, and (iii) ethylene and an alpha-olefin as defined in (a) (ii) containing over 55% of said alpha-olefin, which copolymer is insoluble in xylene at room or ambient temperature; and
 - (c) from 40 to 80 parts of a copolymer fraction wherein the copolymer is selected from the group consisting of (i) ethylene and propylene containing from 20% to less than 40% ethylene, (ii) ethylene, propylene, and an alpha-olefin as defined in (a) (ii), wherein the alpha-olefin is present in an amount of I to 10% and the amount of ethylene and alpha-olefin present is from 20% to less than 40%, and (iii) ethylene and an alpha-olefin as defined in (a) (ii) containing from 20% to less than 40% of said alpha-olefin, and optionally with 0.5 to 10% of a diene, said copolymer fraction being soluble in xylene at ambient temperature, and having an intrinsic viscosity of from 1.5 to 4.0 dl/g;
 - with the total of the (b) and (c) fractions, based on the total olefin polymer composition, being from 50% to 90%, and the weight ratio of(b)/(c) being less than 0.4, wherein said composition has a flexural modulus of less than 150 MPa.
- 4. The film or sheet material of claim 1 or 3, wherein the broad molecular weight distribution propylene polymer material is a propylene homopolymer having xylene insolubles at 25°C greater than or equal to 96 %.

Patentansprüche

1. Film- oder Folienmaterial, umfassend ein Propylenpolymermaterial einer breiten Molekulargewichtsverteilung mit einer Molekulargewichtsverteilung M_w/M_n von 4 bis 20, einer Fließfähigkeit von 0,5 bis 2 dg/Min und einem in Xylol bei 25°C unlöslichen Anteil von mehr als oder gleich 94%, wobei der Film oder die Folie ein-geblasener Film oder

eine geblasene Folie ist.

5

10

15

20

25

30

35

40

- Film- oder Folienmaterial gemäß Anspruch 1, in dem das Propylenpolymermaterial der breiten Molekulargewichtsverteilung ein Propylenhomopolymer einer breiten Molekulargewichtsverteilung oder ein hinsichtlich seiner Schlagzähigkeit mit einem Ethylen/Propylen-Kautschuk modifiziertes Propylenhomopolymer breiter Molekulargewichtsverteilung ist.
- 3. Film- oder Folie gemäß Anspruch 1, bei der das Film- oder Folienmaterial zusätzlich 10% bis 90%, bezogen auf das Gesamtgewicht der Zusammensetzung, einer heterophasischen Olefinpolymerzusammensetzung umfasst, hergestellt durch Polymerisation in mindestens zwei Stufen, und umfassend:
 - (a) 10 bis 50 Teile eines Propylenhomopolymers mit einem isotaktischen Index von mehr als 80, oder eines aus der Gruppe ausgewählten Copolymeren, die besteht aus:
 - (i) Propylen und Ethylen
 - (ii) Propylen, Ethylen und einen α -Olefin der Formel CH $_2$ =CHR, worin R eine gerad- oder verzweigtkettige Alkylgruppe mit 2-8 Kohlenstoffatomen ist, und
 - (iii) Propylen und einem α -Olefin wie in (ii) definiert, wobei das Copolymer über 80% Propylen enthält und einen i-sotaktischen Index von mehr als 80 aufweist;
 - (b) 5-20 Teile einer semikristallinen, im wesentlichen geradkettigen Copolymerfraktion mit einer Kristallinität von 20% bis 60%, wobei das Copolymer aus der Gruppe ausgewählt ist, welche besteht aus (i) Ethylen und Propylen mit einem Gehalt an über 55% Ethylen, (ii) Ethylen, Propylen und einem α -Olefin, wie in (a) (ii) definiert, mit einem Gehalt an 1-10% des α -Olefins und über 55% sowohl an Ethylen als auch dem α -Olefin, und (iii) Ethylen und einem α -Olefin, wie in (a) (ii) definiert, mit einem Gehalt an über 55% an dem α -Olefin, wobei das Copolymer in Xylol bei Raum- oder Umgebungstemperatur unlöslich ist; und (c) 40 bis 80 Teile einer Copolymerfraktion, wobei das Copolymer aus der Gruppe ausgewählt ist, welche besteht aus (i) Ethylen und Propylen mit einem Gehalt an 20% bis weniger als 40% Ethylen, (ii) Ethylen, Propylen und einem α -Olefin, wie in (a) (ii) definiert, wobei das α -Olefin in einer Menge von 1 bis 10% vorliegt, und die vorliegende Menge von Ethylen und α -Olefin 20% bis weniger als 40% beträgt, und (iii) Ethylen und einem α -Olefin, wie in (a) (ii) definiert, mit einem Gehalt an 20% bis weniger als 40% an α -Olefin, und gegebenenfalls mit 0,5 bis 10% eines Diens, wobei die Copolymerfraktion in Xylol bei Umgebungstemperatur löslich
 - und wobei die Summe der Fraktionen (b) und (c), bezogen auf die gesamte Olefinpolymerzusammensetzung, 50 bis 90% beträgt, und das Gewichtsverhältnis von (b)/(c) weniger als 0,4 ist, und die Zusammensetzung einen Elastizitätsmodul von weniger als 150 MPa aufweist.
- Film- oder Folienmaterial gemäß Anspruch 1 oder 3, bei dem das Propylenpolymermaterial breiten Molekulargewichts ein Propylenhomopolymer mit einem in Xylol bei 25°C unlöslichen Anteil von mehr als oder gleich 96% ist.

ist und eine Grenzviskosität von 1,5 bis 4,0 dl/g aufweist;

Revendications

- 45 1. Matière de film ou de feuille comprenant une matière polymère de propylène à large distribution de masse moléculaire ayant une distribution de masse moléculaire M_p/M_n de 4 à 20, un indice de viscosité de 0,5 à 2 dg/min, et une fraction insoluble dans le xylène à 25°C supérieure ou égale à 94%, dans laquelle le film ou la feuille est un film ou une feuille soufflé.
- 2. Matière de film ou de feuille selon la revendication 1, dans laquelle la matière polymère de propylène à large distribution de masse moléculaire est un homopolymère de propylène à large distribution de masse moléculaire, ou un homopolymère de propylène à large distribution de masse moléculaire modifié en résistance au choc par un caoutchouc éthylène/propylène.
- 3. Film ou feuille selon la revendication 1, où la matière de film ou de feuille comprend de plus 10% à 90%, par rapport au poids total de la composition, d'une composition polymère d'oléfine hétérophasique préparée à l'aide d'une polymérisation en au moins deux étapes et comprenant

5

10

15

20

25

30

35

40

45

50

55

(a) de 10 à 50 parties d'un homopolymère de propylène ayant un indice isotactique supérieur à 80, ou un copolymère choisi dans le groupe formé (i) de propylène et d'éthylène, (ii) de propylène, d'éthylène et d'une alpha-oléfine CH₂=CHR, où R est un alkyle en C₂ à C₈ linéaire ou ramifié, et (iii) de propylène et d'une alpha-oléfine telle que définie dans (ii), ledit copolymère contenant plus de 80% de propylène et ayant un indice isotactique supérieur à 80;

(b) de 5 à 20 parties d'une fraction de copolymère semi-cristallin, essentiellement linéaire ayant une cristallinité de 20% à 60%, où le copolymère est choisi dans le groupe constitué (i) d'éthylène et de propylène contenant plus de 55% d'éthylène, (ii) d'éthylène, de propylène, et d'une alpha-oléfine telle que définie dans (a) (ii) contenant de 1 à 10% de l'alpha-oléfine et plus de 55% à la fois d'éthylène et d'alpha-oléfine, et (iii) d'éthylène et d'une alpha-oléfine telle que définie dans (a) (ii) contenant plus de 55% de ladite alpha-oléfine, lequel copolymère est insoluble dans le xylène à la température ambiante ; et

(c) de 40 à 80 parties d'une fraction de copolymère où le copolymère est choisi dans le groupe constitué (i) d'éthylène et de propylène contenant de 20% à moins de 40% d'éthylène, (ii) d'éthylène, de propylène, et d'une alpha-oléfine' telle que définie dans (a) (ii), où l'alpha-oléfine est présente en une quantité de 1 à 10% et la quantité d'éthylène et d'alpha-oléfine présente est de 20% à moins de 40%, et (iii) d'éthylène et d'une alpha-oléfine telle que définie dans (a) (ii) contenant de 20% à moins de 40% de ladite alpha-oléfine, et éventuellement avec 0,5 à 10% d'un diène, ladite fraction de copolymère étant soluble dans le xylène à température ambiante, et ayant une viscosité intrinsèque de 1,5 à 4,0 dl/g;

le total des fractions (b) et (c), par rapport à la composition de polymère d'oléfine totale, étant de 50% à 90%, et le rapport pondéral de (b)/(c) étant inférieur à 0,4, où ladite composition possède un module en flexion inférieur à 150 MPa.

4. Matière de film ou de feuille selon la revendication 1 ou 3, dans laquelle la matière polymère de propylène à large distribution de masse moléculaire est un homopolymère de propylène ayant une fraction insoluble dans le xylène à 25°C supérieure ou égale à 96%.